

1 Phase change dynamics in a cylinder containing hybrid
2 nanofluid and phase change material subjected to a
3 rotating inner disk

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15 **Abstract**

16 In this numerical study, the phase change dynamics of a 3D cylinder con-
17 taining hybrid nanofluid and phase change material (PCM) is investigated
18 with a finite element solver. The PCM consists of spherical encapsulated
19 paraffin wax, and the flow is under the forced convection regime. The dy-
20 namic features of the phase change process are studied for different values of
21 the Reynolds number (between $Re=100$ and 300), the rotational Reynolds
22 number of the inner disk ($Re_w=0$ and 300), and the size of the rotating disk
23 (length between $0.1L$ and $0.55L$; height between $0.001H_2$ and $0.4H_2$). The
24 flow dynamics and separated flow regions are found to be greatly influenced
25 by the rotational speed and size of the inner disk. As Re is increased, the
26 difference between the transition times at different rotational disk speeds de-
27 creases. At $Re=100$, a 21% reduction in the phase transition time is observed

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28 when the inner disk rotates at the highest speed as compared to the motion-
 29 less case. Up to a 26% variation in the phase transition time occurs when
 30 the size of the inner rotating disk is varied. A 5 input-1 output feed-forward
 31 artificial neural network is applied to achieve fast and reliable predictions of
 32 the phase change dynamics. This study shows that introducing rotational
 33 effects can have a profound effect on the phase change dynamics of a hybrid
 34 nanofluid system containing phase change material.

35 *Keywords:* rotational surface, phase change, CFD, finite element method,
 36 artificial neural network, hybrid particles

Nomenclature

k thermal conductivity

H cylinder height

L cylinder length

L_f latent heat of fusion

n unit normal vector

37 Nu Nusselt number

p pressure

$L_{1,2}$ disk radius

Pr Prandtl number

Re Reynolds number

Re_w rotational Reynolds number

t time

T temperature

T_m melting temperature

u, v, w velocity components

r, z cylindrical coordinates

Greek Characters

ν kinematic viscosity

ρ density of the fluid

ϕ solid volume fraction

ω rotational speed

Subscripts

c cold

h hot

m average

nf nanofluid

p solid particle

38 **1. Introduction**

39 Energy applications involving phase change material (PCM) equipped
40 products have been gaining attention recently due to their performance en-
41 hancement potential. Thermal energy (TE) storage and management are
42 two major areas that are applicable to various energy systems such as in
43 solar power, refrigeration, electronic cooling, waste heat recovery, building
44 energy, agriculture and many others. Due to the low cost and favorable
45 heat transfer (HT) characteristics, packed bed latent heat storage (HS) is
46 considered a promising technology. Many methods can improve the per-
47 formance features of PCM embedded TE systems. In the review of Khan
48 et al. [1], different methods for influencing the thermo-physical properties
49 of PCMs were presented such as using fins, high conductivity additives and
50 various arrangement of PCMs in TE systems. Thermal utilization of PCM
51 was explored by considering different techniques and accounting for stabil-
52 ity issues. Sharma et al. [2] reviewed PCM installed TE systems in diverse
53 applications such as in waste heat, building and solar air heaters. Enhanc-
54 ing the thermal performance of PCMs by using internal fins, metallic foams
55 and nano particles was considered in the review by Sahoo et al. [3]. Heat
56 sinks with PCM enhancement techniques were considered for constant and
57 variable loads while metallic foams offered several advantageous. Fins with
58 PCM have been considered in heat sinks [4, 5], photovoltaic panels [6, 7] and
59 building applications [8, 9].

60 Recently, nano-sized particles have been used in HT fluids for TE systems
61 to improve performance. Many nanofluid types have been evaluated and ex-
62 perimental correlations for the effective thermophysical properties have been

63 derived [10]. Many advanced simulation methods have been developed and
64 tested for accurate modeling of TE systems using nanofluids [11–15]. The
65 utilization of nanotechnology in PCM embedded systems has been consid-
66 ered in various TE systems [16]. In the review of Rostami et al. [17], PCM
67 characteristics including nano-PCMs on TE storage and natural convection
68 were critically discussed. Through numerical simulations, Khodadadi and
69 Hosseinizadeh [18] showed performance improvement for freezing of water
70 by using CuO nanoparticles in a cavity with numerical simulations. Other
71 studies that have considered the use of nanoparticles with PCM can be found
72 in Refs. [19–27].

73 The performance of PCM embedded systems can be enhanced by chang-
74 ing the geometrical features along with the thermophysical properties of the
75 HT fluid. In TE systems with embedded latent heat storage units with
76 encapsulated PCM, dynamic walls can be implemented to improve the per-
77 formance. Rotating surfaces have been considered in many TE systems espe-
78 cially for convective HT applications. Although the thermal system perfor-
79 mance can be improved via passive methods such as changing the geometry
80 of the TE systems and installing static elements such as internal fins, metal
81 foams, the use of dynamic walls or objects opens up new opportunities for
82 further improvements. A rotating type object has been shown to affect the
83 convective HT thermal performance via adjustments in the rotational speed,
84 size and location of the object [28, 29]. Certain locations and rotational
85 direction of the cylinder have been found to assist the convection in TE sys-
86 tems. The combined effects of using nanofluids and surface rotations have
87 been considered in many studies for HT improvement in TE systems [30, 31].

88 The present work considers the effects of using a rotating inner disk on the
89 performance of a PCM embedded thermo-fluid system. The effects of rotation
90 of the inner disk and of its geometrical parameters on the dynamic features
91 of the phase change process are numerically assessed. The effects of fluid
92 velocity and its interaction with the rotation of the inner disk surface on the
93 flow features are analyzed. The numerical simulations are validated against
94 an experimental study of the phase change process. With the diverse use of
95 PCMs in TE systems such as in electronic cooling, solar energy applications,
96 heat exchangers, the thermal management of the phase change process via a
97 rotating inner disk and nanofluid is novel and may be used to enhance the
98 performance of PCM embedded energy systems.

99 **2. Computational study**

100 **2.1. System configuration**

101 The characteristics of a PCM-equipped cylinder under the effects of a
102 rotating inner disk is analyzed. The height and radius of the PCM included
103 region is h_{pcm} and L . The rotating disk has inner and outer radius of $L1d$
104 and $L2d$ while heights are $H1d$ and $H2d$. The rotational speed (R_s) of the
105 inner disk is ω . Here, $H1$ and $H2$ denote the distance of the PCM region
106 from the outlet and inlet, respectively. A hybrid nanofluid (with Ag and
107 MgO nanoparticles at solid volume fraction of 2%) enters the cylinder with
108 a velocity of u_g and a temperature of T_g . Experimental correlations for the
109 effective nanofluid properties were used as given in [32]. Spherical shaped
110 encapsulated paraffin wax is considered as the PCM with a radius of 30 mm.
111 Table 1 lists the thermophysical properties.

112 **2.2. Governing equations and boundary conditions**

113 A single phase model of nanofluid is used with Newtonian and incompress-
 114 ible fluid assumptions. Effects such as free convection, thermal radiation and
 115 viscous dissipation are ignored.

116 A hybrid nanofluid containing binary particles of Ag and MgO was used.
 117 The potential of using hybrid nanofluids has been shown in various studies
 118 of thermal engineering. They are preferred for their synergistic effects, cost
 119 and advantages of one or more types of nanoparticles in the base fluid [33–
 120 36]. In studies with nanofluid, an accurate description of the thermophysical
 121 properties is important. The experimental data fit from Ref.[32] was used to
 122 derive correlations for the thermal conductivity (k_{nf}) and viscosity (μ_{nf}) of
 123 the hybrid nanofluid. They are defined as [32]:

$$124 \quad k_{nf} = \left(\frac{0.1747 \times 10^5 + \phi}{0.1747 \times 10^5 - 0.1498 \times 10^6 \phi + 0.1117 \times 10^7 \phi^2 + 0.1997 \times 10^8 \phi^3} \right) k_f, \quad (1)$$

$$\mu_{nf} = (1 + 32.795\phi - 7214\phi^2 + 714600\phi^3 - 0.1941 \times 10^8 \phi^4) \mu_f. \quad (2)$$

125 where ϕ is the the total concentration of nanoparticles and is taken as 2%.

126 In the fluid domain, the conservation equations are [37]:

$$\nabla \cdot \mathbf{u} = 0 \quad (3)$$

$$127 \quad \rho(\mathbf{u} \cdot \nabla) \mathbf{u} = \nabla \cdot [-p\mathbf{I} + \mathbf{K}] + F \quad (4)$$

$$\mathbf{K} = \mu \left(\nabla \mathbf{u} + (\nabla \mathbf{u})^T \right)$$

$$128 \quad \rho C_p \frac{\partial T}{\partial t} + \rho C_p \mathbf{u} \cdot \nabla T = \nabla \cdot (k \nabla T) \quad (5)$$

129 For the PCM region:

$$\nabla \cdot \mathbf{u} = 0 \quad (6)$$

130

$$\frac{1}{\varepsilon_p} \rho (\mathbf{u} \cdot \nabla) \mathbf{u} \frac{1}{\varepsilon_p} = \nabla \cdot [-p \mathbf{I} + \mathbf{K}] - (\mu \kappa^{-1} + \beta_p \rho |\mathbf{u}|) \mathbf{u} + F$$

$$\mathbf{K} = \mu \frac{1}{\varepsilon_p} \left(\nabla \mathbf{u} + (\nabla \mathbf{u})^T \right) \quad (7)$$

131 and with the Kozeny-Carman permeability given as:

$$\kappa = \frac{d_p^2}{180} \frac{\varepsilon_p^3}{(1 - \varepsilon_p)^2} \quad (8)$$

132 A phase change function α is defined with a value of 0 for $T < (T_m - \Delta T_m/2)$ 133 and 1 for $T > (T_m + \Delta T_m/2)$. The energy equation is given as:

$$\rho C_p \frac{\partial T}{\partial t} + \rho C_p \mathbf{u} \cdot \nabla T = \nabla \cdot (k \nabla T). \quad (9)$$

134 with the thermo-physical properties as:

$$\theta = 1 - \alpha, \quad \rho = \theta \rho_{f1} + (1 - \theta) \rho_{f2},$$

$$C_p = \frac{1}{\rho} (\theta \rho_{f1} C_{p,f1} + (1 - \theta) \rho_{f2} C_{p,f2}) + L \frac{\partial \alpha_m}{\partial T}, \quad (10)$$

$$k = \theta k_{f1} + (1 - \theta) k_{f2}, \quad \alpha_m = \frac{1(1 - \theta) \rho_{f2} - \theta \rho_{f1}}{2 \theta \rho_{f1} + (1 - \theta) \rho_{f2}}.$$

135 In the above derivation, $f1$, $f2$ and L are the phases and latent heat of

136 fusion. In between the phases, non-equilibrium HT in porous media interface

137 is considered. Here, two equations for the phases and additional source terms

138 are given [38, 39]:

$$\theta_p \rho_s C_{p,s} \frac{T_s}{\partial t} + \nabla \cdot \mathbf{q}_s = q_{sf} (T_f - T_s) + \theta_p Q_s, \quad (11)$$

139

$$\mathbf{q}_s = -\theta_p k_s \nabla T_s, \quad (12)$$

140

$$(1 - \theta_p) \rho_f C_{p,f} \frac{T_f}{\partial t} + (1 - \theta_p) \rho_f C_{p,f} \mathbf{u}_f \cdot \nabla T_f +$$

$$+ \nabla \cdot \mathbf{q}_f = q_{sf} (T_s - T_f) + (1 - \theta_p) Q_f, \quad (13)$$

141

$$\mathbf{q}_f = -(1 - \theta_p)k_f \nabla T_f. \quad (14)$$

142 In the above equations, \mathbf{q}_f , \mathbf{q}_s , θ_p denote the conductive heat fluxes of the solid
 143 and fluid and porous media SVF. The interstitial convective HT coefficient
 144 is given by the term q_{sf} while Q_s and Q_f are the solid and fluid heat sources,
 145 respectively. For a spherical pellet bed [38, 39]:

$$q_{sf} = a_{sf}h_{sf} \quad (15)$$

146 The interstitial HT coefficient is given by [38, 39]:

$$\frac{1}{h_{sf}} = \frac{2r_p}{k_f \text{Nu}} + \frac{2r_p}{\beta k_s}. \quad (16)$$

147 The value of β is taken to be 10 for spherical particles. The fluid-to-solid Nu
 148 number is: [40]:

$$\text{Nu} = 2 + 1.1\text{Pr}^{1/3}\text{Re}_p^{0.6}. \quad (17)$$

149 The Prandtl number and Reynolds number of the particles are:

$$\text{Pr} = \frac{\mu C_{p,f}}{k_f}, \quad \text{Re}_p = \frac{2r_p \rho_f |u_f|}{\mu}. \quad (18)$$

150 The relevant non-dimensional parameters are the Reynolds number (Re)
 151 for the fluid and the rotational Reynolds number (Rew) for the rotating inner
 152 disk, both of which are varied in our simulations. They are given as:

$$\text{Re} = \frac{u_g L \rho}{\mu}, \quad \text{Rew} = \frac{\omega (L1d)^2 \rho}{\mu} \quad (19)$$

153 The Re number and rotational Re of the inner disk are the varied during
 154 the simulation. The fluid velocity at the inlet is u_g and the temperature is
 155 $T_g=336$ K. The model is axis-symmetrical with $\frac{\partial T}{\partial r} = 0$. The walls of the

156 cylinder are adiabatic with no-slip boundary conditions (BCs) as, $u = w = 0$,
 157 $\frac{\partial T}{\partial n} = 0$. A pressure outlet is used at the exit. The inner disk is rotating with
 158 Rs of ω . The velocity of the tangentially moving wall is 0 while the angular
 159 component of the moving wall is ωr . The rotating disk is also considered
 160 adiabatic such that $\frac{\partial T}{\partial n} = 0$ with an initial temperature of 303 K.

161 2.3. Solution method and code validations

162 To solve the above GEs, the GWR-finite element method is used. The
 163 field variable (ψ) appropriations are performed as:

$$\psi = \sum_{n=1}^{N^s} \Phi_n^s \Psi_n \quad (20)$$

164 where Φ^s is the shape function and Ψ is the element nodal value. Different
 165 ordered Lagrange FEM is considered. The time dependent part is treated
 166 by utilizing a second order backward differentiation scheme. A time step
 167 size of 0.1 min is used. Time step independence of the solution is also as-
 168 sured. A commercial computational fluid dynamics code Comsol was used
 169 with built-in modules for multi-physics simulations [39]. Tests for grid inde-
 170 pendence were conducted and the results are given in Figure 2 (a) for two
 171 different values of Rs of the inner disk. Grid system G4 with 63412 elements
 172 is selected. At the interface regions and near the walls, the mesh is finer
 173 as shown in Figure 2 (b). Validation is conducted by using results for the
 174 phase change process and impacts of rotation on the convective HT. First,
 175 results available in Ref. [41] are used. In the study, experimental analysis for
 176 PC process in a differentially heated cavity was performed. The role of free
 177 convection for PC of pure metal was explored while the two vertical walls of
 178 the rectangular test section were maintained at different temperatures. The

179 amount of solidified volume is a time dependent quantity and it depends on
 180 the solidified volume (V), Rayleigh number (Ra), total volume (V_0), aspect
 181 ratio (AT) and dimensionless time (τ) as:

$$\frac{V}{V_0} = 2.91\tau^{0.53}Ra^{-0.05}A^{-0.36} \quad (21)$$

182 Figure 3 compares the solidified volume at different dimensionless times Com-
 183 pared with experimental data, the greatest difference observed as -9.3% at
 184 $\tau^{0.53}Ra^{-0.05}A^{-0.36} = 0.114$. In another study, Roslan et al. [42] explored the
 185 effects of rotation on convective HT by using an inner cylinder in square cav-
 186 ity. They considered a differentially heated enclosure while rotational speed
 187 and size effects of the inner cylinder on the convective HT features were ex-
 188 plored using FEM. Comparison of the average Nu is given in Figure 5 for two
 189 different configurations (cylinder size and Rs). In both cases, the difference
 190 is limited to under 3%. The results reinforce the capability of the code in
 191 simulating the PC process and the rotational effects of the inner surfaces on
 192 convection.

193 **2.4. Performance estimation with artificial neural network**

194 Artificial neural network (ANN) modeling is widely used in energy sys-
 195 tems and thermal engineering for flow control, performance prediction and
 196 system identification. Many different soft computing methods and ANN
 197 techniques have been demonstrated for accurate performance predictions of
 198 energy systems [43–49]. Many steps involved in soft computing methods are
 199 similar such as specification of the input-output data set, activation func-
 200 tions, learning algorithms and validation tests. The Levenberg-Marquardt

201 (LM) techniques with backpropagation (BP) is chosen here as learning algo-
 202 rithm [50]. A mathematical model for the input-output relation of the data
 203 set can be derived with an ANN. The network structure consists of multiple
 204 different layers (input, hidden and output layers) and different numbers of
 205 neurons are used in the hidden layers. They can be adjusted along with the
 206 network parameters during the training phase. The network performance at
 207 each iteration step is checked by comparing the network output and data
 208 from simulations or experiments while the weights of the ANN are updated.
 209 A learning algorithm with backpropagation is used for adjusting the weights
 210 of ANN. Each neuron output is given as [47]:

$$Y = G \left(\sum_{i=1}^M X_i W_i + S \right) \quad (22)$$

211 where Y, G and M represent the output data, activation function and data
 212 number while X, W and S are the input, weight and bias term, respectively.
 213 Different criteria may be applied to test the performance of different ANN
 214 models. The mean square error (MSE) and coefficient of determination (R^2)
 215 are commonly used [51]:

$$\text{MSE} = \frac{1}{M} \sum_{i=1}^M (y_i^{CFD} - y_i^N)^2, \quad (23)$$

216

$$R^2 = 1 - \frac{\sum_{i=1}^M (y_i^{CFD} - y^N)^2}{\sum_{i=1}^M (y_i^{CFD} - \bar{y}^N)^2}. \quad (24)$$

217 3. Results and discussion

218 The effects of using a rotating object in a PCM filled cylinder on the
 219 performance enhancement are numerically assessed. The Rs of the disk is ω

220 and is varied during the simulation. The dynamic characteristics of the phase
221 change process are studied for various values of Re (between 100 and 300),
222 Re_w of the disk (0 and 300), and size of the rotating disk (length between
223 $0.1L$ and $0.55L$; height between $0.001H_2$ and $0.4H_2$). The time evolution of
224 the liquid fraction (L_f) and phase completion time are analyzed. ANN-based
225 estimation is performed to determine the time dependent characteristics of
226 the liquid fraction for various values of input parameters such as Re_w and
227 the size of the inner rotating disk.

228 3.1. *CFD simulation results*

229 Figure 5 shows the impacts of Re on the flow patterns variation at two
230 different values of Re_w . When the inner disk is not rotating, the flow sep-
231 arates at the edge of the disk away from the inlet and its extent increases
232 with Re . However, in the presence of rotational effects due to the inner disk
233 surfaces, the separated flow region extending through the PCM domain be-
234 comes significant. As Re is increased, the size of the vortex at the interface
235 becomes reduced and the recirculation zone is suppressed. The recirculation
236 zone becomes larger at the edges of the rotating disk as Rs increases (Figure
237 6). The separated flow region moves toward the vertical wall of the cylin-
238 drical container for higher Re_w . Time evolutions of the PCM temperatures
239 for different Re_w are presented in Figure 7. Due to the recirculation zones
240 caused by rotation of the inner disk, the PCM temperatures are significantly
241 affected in the inner part and toward the walls when the disk is rotating at
242 the highest speed. Variation of the PCM temperatures at two points (in the
243 axis- symmetric location and in the vertical wall) are shown in Figure 8 for
244 various values of Re and Rs of the inner disk. In the absence and presence of

245 rotational effects, when the fluid velocity increases, the phase change process
246 speeds up. However, the effects of Rw on the phase change differs at the mid
247 point (axis-symmetrical location) and in the wall location. At the wall loca-
248 tion, phase transition becomes rapid with increasing Rw while the effects is
249 reversed at mid point location. Time evolution of the liquid fraction at two
250 different values of Rw is given in Figure 9. At $t=40$ min full phase transi-
251 tion is achieved when rotational effects of the inner disk are considered at the
252 highest speed. Near the wall region and interior of the cylinder, rotational
253 effects on the phase transition become dominant. The dynamic characteris-
254 tics of the liquid fraction (Fr) for various Re at two different values of Rw
255 of 0 and 300 are shown in Figure 10. The values of Fr approach for higher
256 Re for both values of Rw . A saturation type curve is obtained while the
257 discrepancy between different Re on Fr becomes different when rotational
258 effects are considered. Full phase transition time (tr) with different Re and
259 Rw are given in Figure 11. The effects of Rw on tr becomes dominant for
260 lower fluid velocities but at $Re=300$, its impacts are negligible. There is a
261 21% reduction in the full transition time at $Re=100$ when rotational effects
262 at the highest speed are considered as compared to a motionless disk. When
263 the effects of Rw are considered, the full phase transition time first increases
264 up to $Rw=50$ but decreases thereafter. This is attributed to the balance
265 between vortex formation which has negative effects on the phase change
266 process while for higher rotational speeds, the fluid velocity near the rota-
267 tion surfaces becomes higher, causing a positive impact on the phase change
268 process. There is almost a 16 % reduction in tr when the configuration with
269 higher Rs is compared with the case of a motionless disk.

270 Geometrical parameters of the rotating disk have also affected the phase
271 change process. The flow pattern variations with varying length and height of
272 the rotating disk are given in Figure 12. The separated flow region becomes
273 significant and occupies a large portion of the PCM region for $L2d=0.3L$
274 while it is smallest for $L2d=0.1L$. At $L=0.55L$, the region approaches the
275 vertical wall of the cylinder. When the height is increased, an elongation of
276 the vortex region in the flow direction is observed. At the highest height,
277 its size is reduced in the radial direction. Varying the length and height of
278 the rotating inner disk has opposite effects when the time evolution of the
279 temperatures at the wall region is compared to the location at the mid-axis
280 plane. At the wall location, the phase change process becomes faster for
281 higher values of length and height of the inner rotating disk. The dynamic
282 features of liquid fraction are highly affected with varying length as compared
283 to height (Figure 14). The Fr values become lower with higher length of the
284 rotating disk most of the time. Full phase transition shows non-monotonic
285 behavior with varying geometrical parameters of the inner disk. When the
286 length is increased up to $L2d=0.3L$, the value of tr is reduced, indicating that
287 the phase change process is relatively fast. Even though the recirculation
288 region becomes larger, due to the increased fluid velocity with rotation, it
289 is lower. However, for disk lengths greater than $L2d=0.3L$, the value of tr
290 increases, a trend attributed to the movement of the vortex region toward
291 the vertical walls, resulting in an inefficient phase change process. There is
292 a 26% reduction in the value of tr when cases with $L2=0.1H$ and $L2=0.3H$
293 are compared. When the height is increased to $H2d=0.1L$, the value of
294 tr reduces owing to a reduction of the vortex size in the radial direction.

295 However, further increases of the rotating disk height resulted in longer full
296 phase transition times. The variation in the tr values becomes 21% while the
297 lowest tr value is achieved at $H2d=0.1H2$.

298 3.2. ANN prediction

299 Feed-forward ANNs are used for performance predictions and dynamic
300 feature extraction of the PCM-equipped energy system with a rotating disk.
301 As input, five input data is selected. They are Re, Rew, height /length of
302 the rotating disk and time (t in minutes). As network output, the liquid
303 fraction (Lr) is selected. Here, 1877 CFD simulation datasets are generated
304 with 70% used for training and the remainder used for testing and vali-
305 dation. As the activation function, a hyperbolic tangent sigmoid function
306 ($f(x) = 1/(1 + e^{-x})$) is used while LM-BP is selected as the learning algo-
307 rithm. The number of neurons in the hidden layer is determined according
308 to their performances in the hidden layer; it is chosen to be 15 (Table 2) for
309 training. Figure 16 shows a schematic view of the ANN structure with differ-
310 ent layers and network features. ANN performance with 15 neurons and for
311 various data sets (training, validation and testing) is given in Table 3. Lower
312 values of MSE are obtained while R^2 approach 1. Comparison of network
313 performance estimation for various Rew of the inner disk is given in Figure
314 18 (a). Effects of varying the length of the rotating disk on the full phase
315 transition time is given in Figure 18 (b) by using CFD simulation and ANN
316 estimation model. These results show that the ANN model has higher pre-
317 diction accuracy when analyzing the effects of using inner rotating cylinder
318 on the phase change dynamics. Variations of the full phase completion time
319 and and time dependent variation of the liquid fraction can be estimated by

320 using the ANN model where time is used as an additional parameter.

321 4. Conclusions

322 In the present study, the effect of using a rotating inner disk on the
323 performance of a PCM-equipped thermo-fluid system containing a hybrid
324 nanofluid. The following conclusions can be drawn as:

- 325 • Introducing rotational surface effects of the inner disk significantly af-
326 fected the flow features. There is a 21% reduction in the phase tran-
327 sition time at $Re=100$ when the inner disk is rotating at the highest
328 speed as compared to the motionless cases.
- 329 • Vortex formation occurs within the system at higher rotational speeds
330 due to the resultant changes in the phase change process. At higher
331 Re_w , the phase change process is accelerated with up to a 16 % reduc-
332 tion in the transition time
- 333 • Separated flow zones occupying the PCM region are affected by the
334 size of the rotating inner disk.
- 335 • The dynamic properties of the liquid fraction are influenced more by
336 varying the length than by varying the height of the inner disk. When
337 configurations at disk sizes of $L_2=0.1H$ and $L_2=0.3H$ are compared,
338 there is a 26% reduction in the phase transition time but this drops to
339 21% when varying the height of the rotating disk.
- 340 • Feed-forward ANN modeling with 15 neurons in the hidden layer is
341 shown to provide fast and accurate estimation results.

342 In future work, this study can be extended to include different thermal
343 boundary conditions, different PCMs, geometric modifications in the main
344 reactor and the PCM region, effects of HT fluid inlet temperature varia-
345 tions and using various types of hybrid nanofluids. This should increase the
346 applicability of the present results.

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Table 1: Thermo-physical properties of PCM

Property	Value
Melting temperature (T_m , °C)	60
Latent heat of fusion (L, kJ/kg)	213
Density-solid (ρ , kg/m ³)	861
Density-liquid (ρ , kg/m ³)	778
Thermal conductivity-solid (k, W/m°C)	0.40
Thermal conductivity-fluid (k, W/m°C)	0.15
Specific heat-solid (C_p , J/kg°C)	1850
Specific heat-fluid (C_p , J/kg°C)	2384

Table 2: Network performance dependence on the neuron in the hidden layer

Number of neurons	MSE -Training	R ² -Training
10	6.806×10^{-4}	0.9973
15	1.102×10^{-4}	0.9995
25	2.767×10^{-4}	0.9986

Table 3: ANN results for training, testing and validation using 15 neurons in the hidden layer

Data Type	Number of samples	MSE	R ²
Training	1313	1.102×10^{-4}	0.9995
Validation	282	1.287×10^{-4}	0.9994
Testing	282	1.467×10^{-4}	0.9994

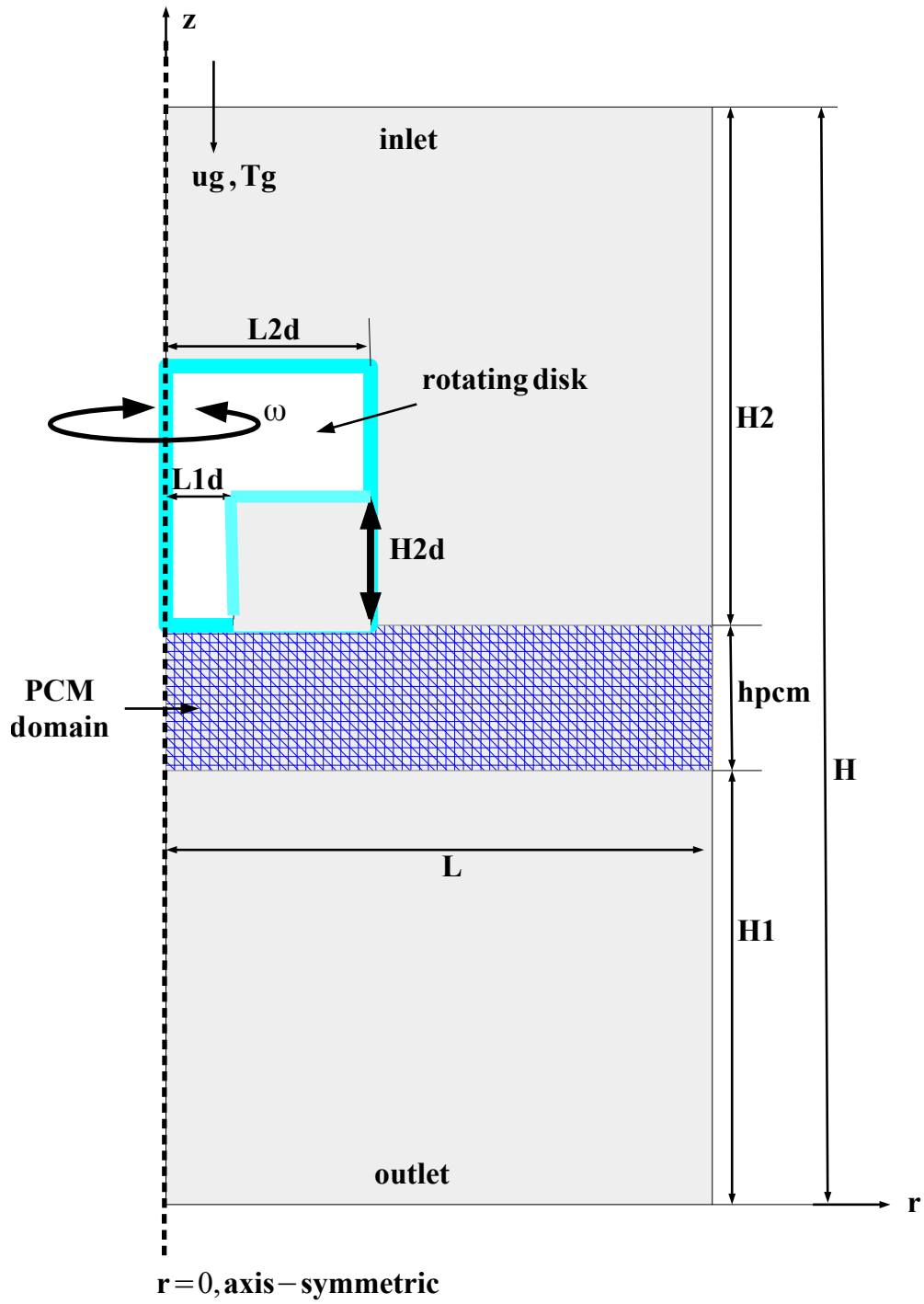
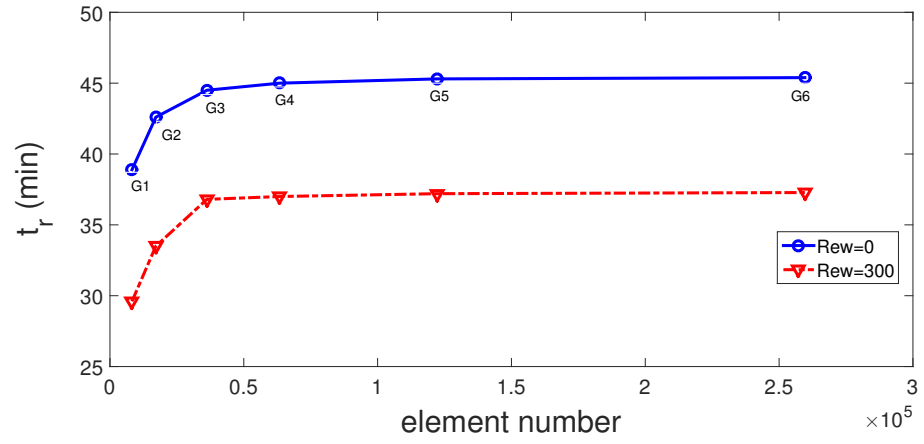
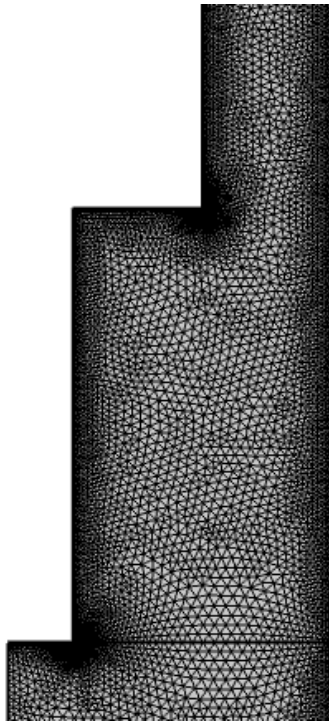


Figure 1: PCM equipped cylinder with a rotating inner disk



(a)



(b)

Figure 2: Numerical results for grid independence at two different values of Re_w (a) ($Re = 200, L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$) and distribution of grid (b)

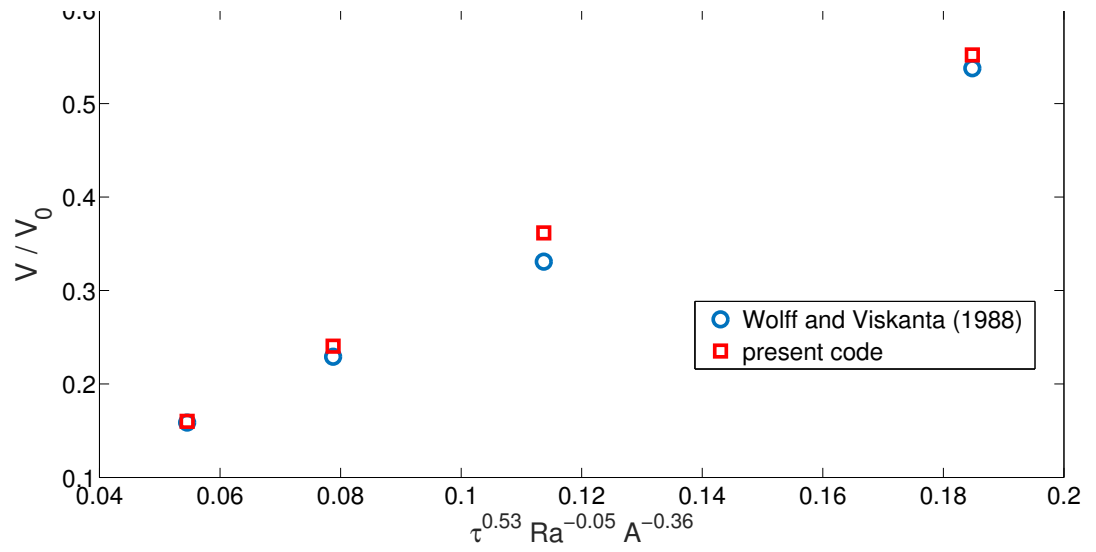


Figure 3: Comparisons of solidified volume fraction for data available in Ref. [41]

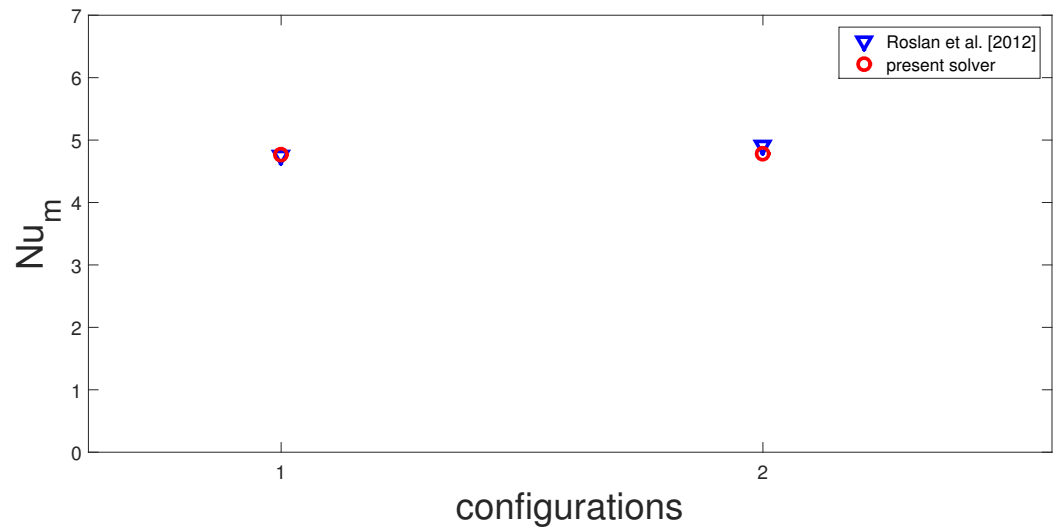


Figure 4: Average Nu comparison in a cavity with an inner rotating cylinder (configuration 1: $R=0.1$, $\Omega = 500$ and configuration 2: $R=0.2$, $\Omega = 1000$, Reference values in [42] were used.)

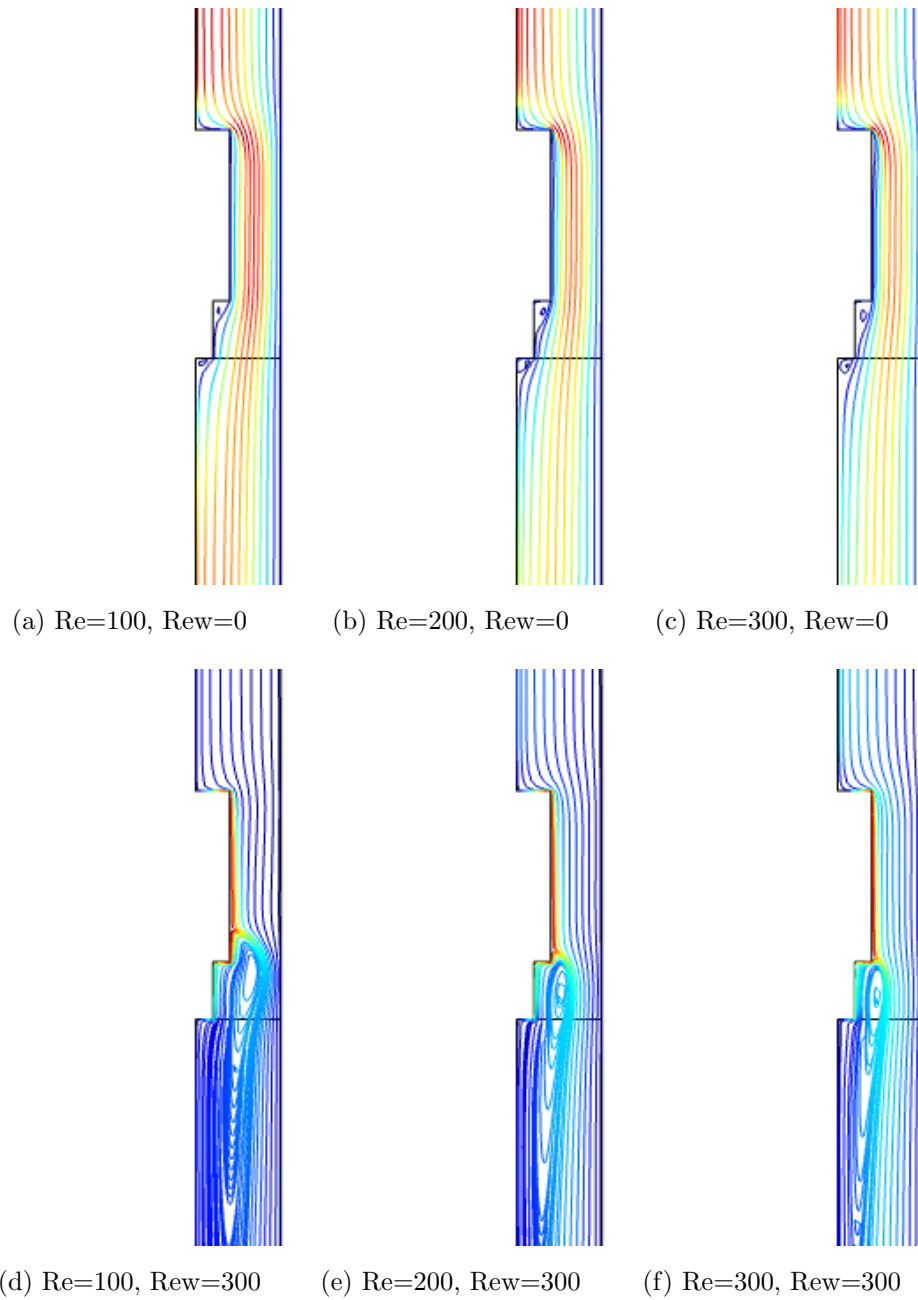


Figure 5: Influence of Re on the flow patterns at two different values of Rew ($L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)

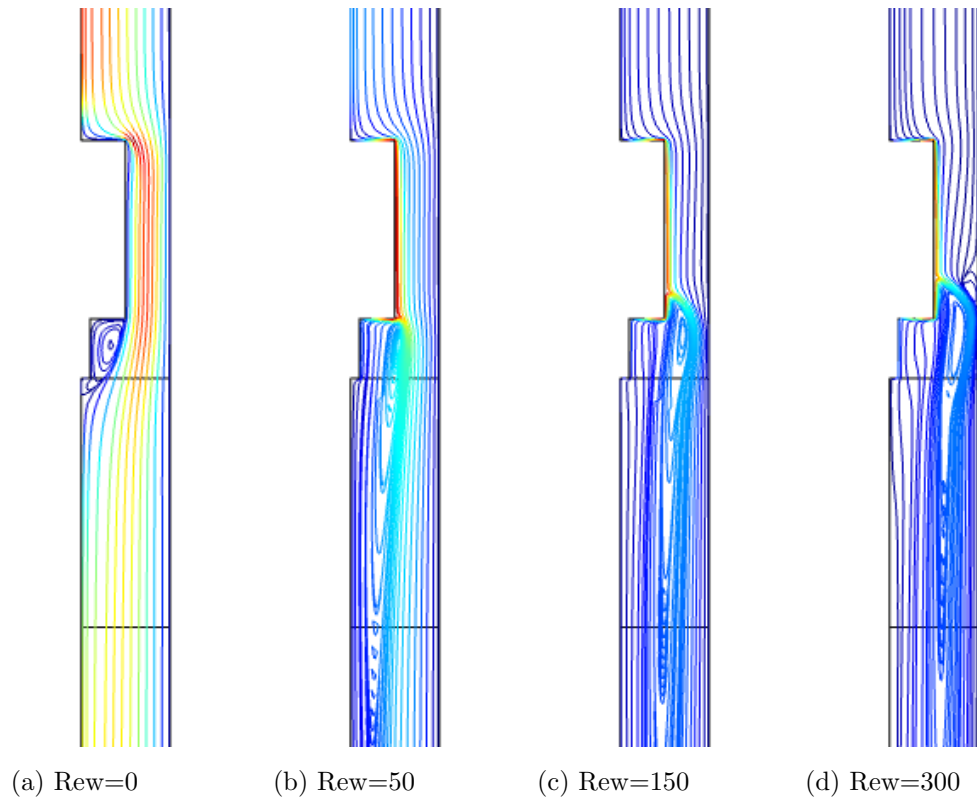


Figure 6: Effects of Re_w on the flow patterns ($Re = 200, L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)

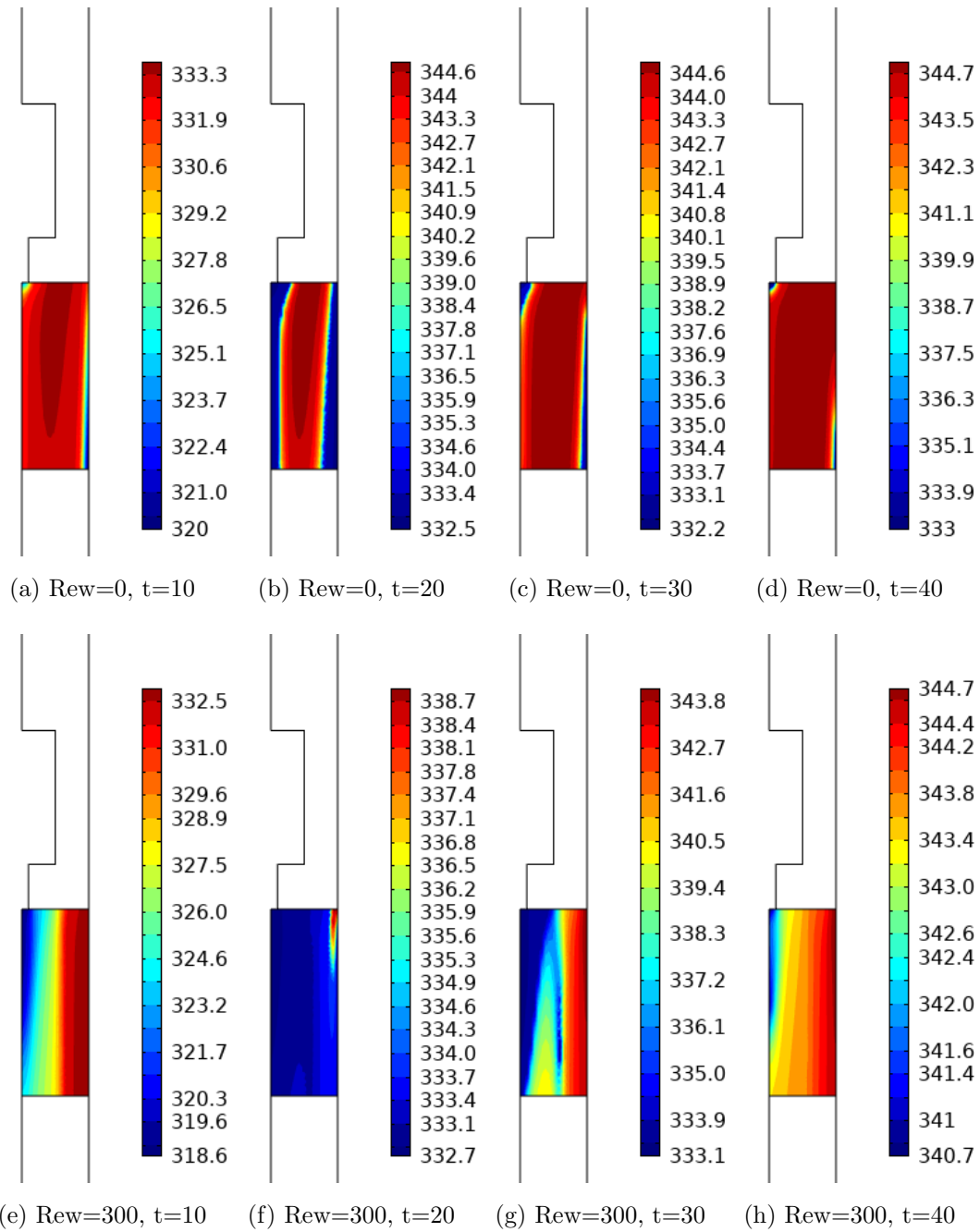
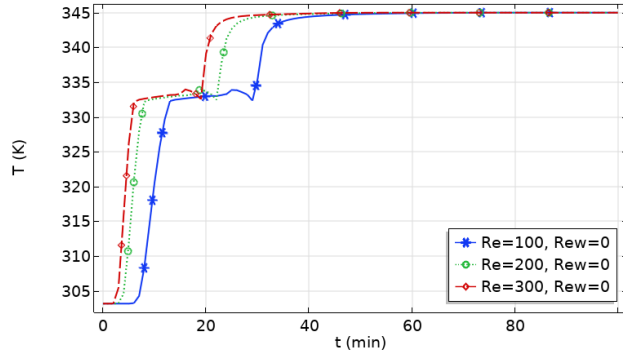
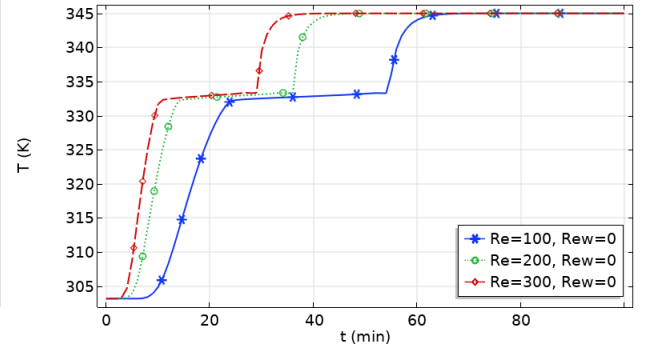


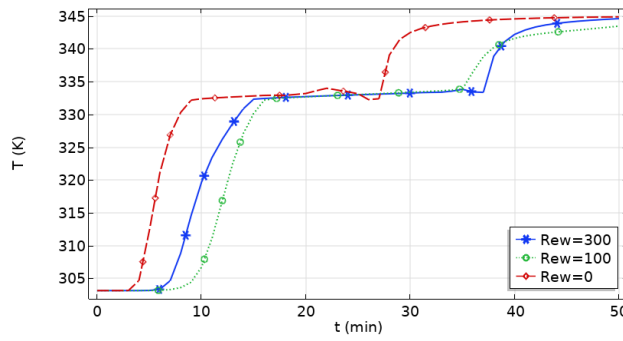
Figure 7: Effects of Re_w on T_p at various time instants in minutes ($Re = 200, L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)



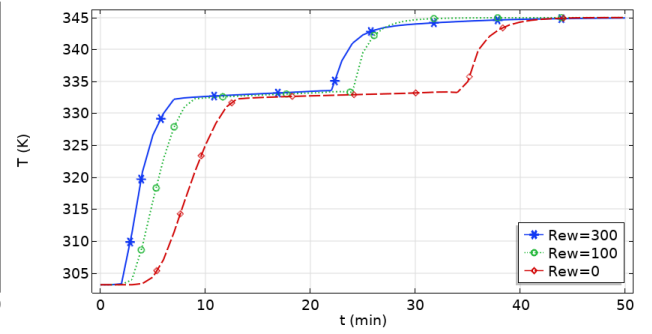
(a) $Rew=0$, mid point



(b) $Rew=300$, wall point

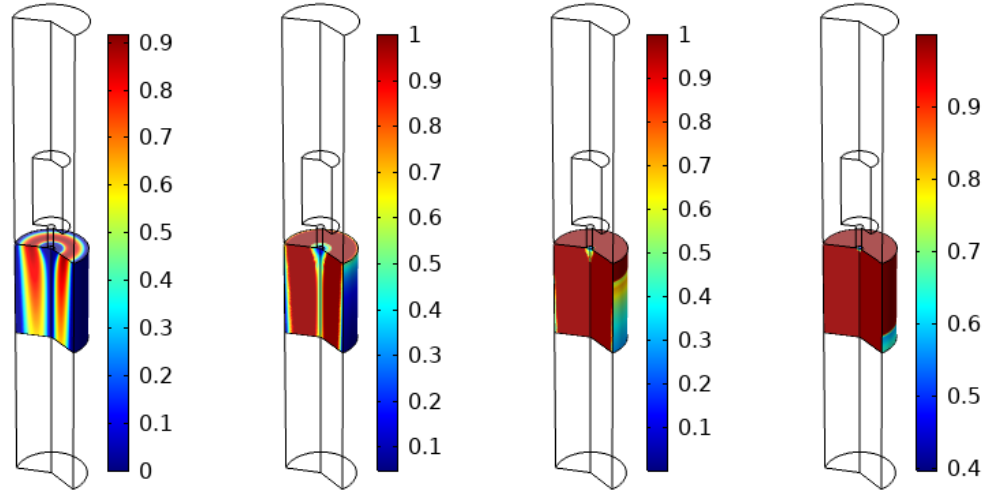


(c) $Re=200$, mid point

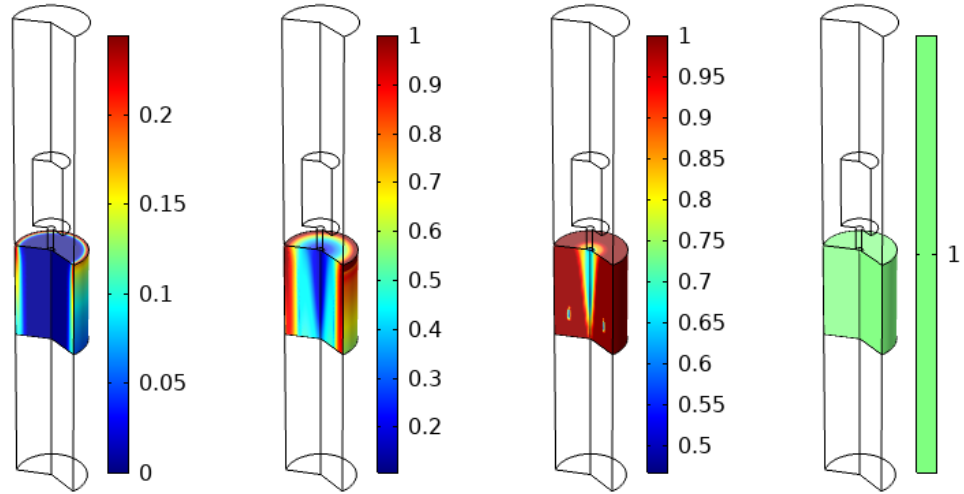


(d) $Re=200$, wall point

Figure 8: Influence of Re and Rew on the PCM temperature at two different points
 ($Re = 200$, $L1d = 0.1L$, $L2d = 0.5L$, $H2d = 0.3H2$)

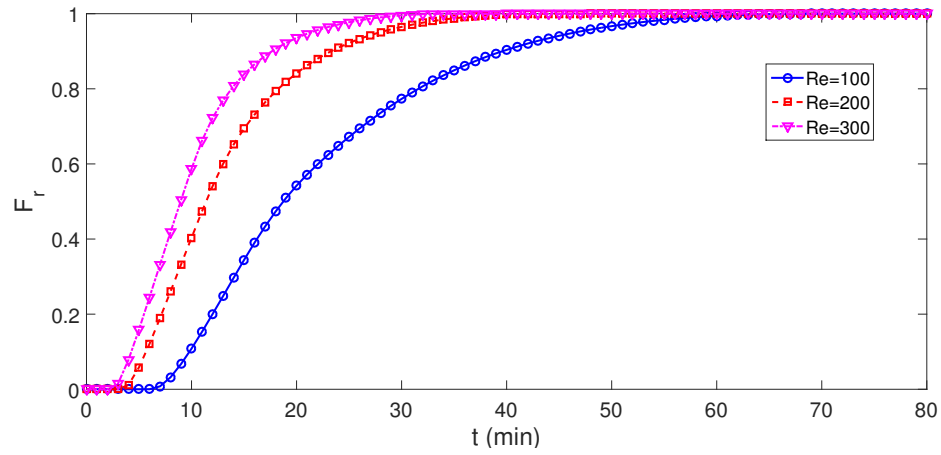


(a) $Re=0, t=10$ (b) $Re=0, t=20$ (c) $Re=0, t=30$ (d) $Re=0, t=40$

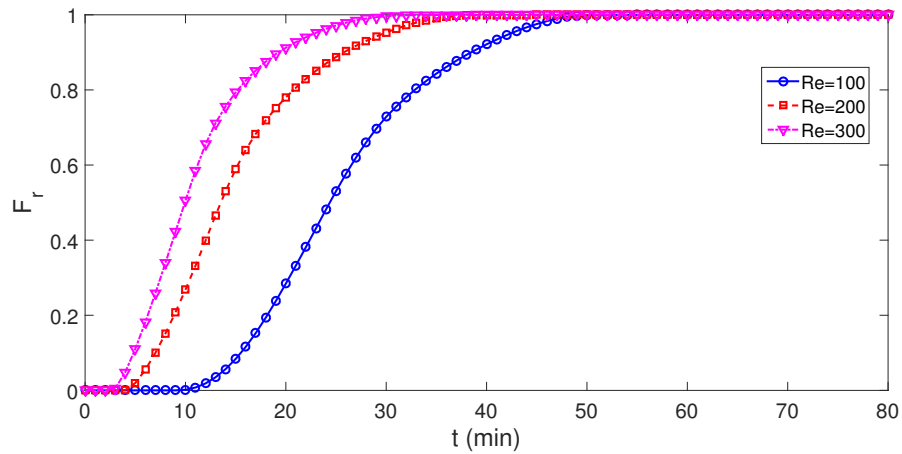


(e) $Re=300, t=10$ (f) $Re=300, t=20$ (g) $Re=300, t=30$ (h) $Re=300, t=40$

Figure 9: Effects of Re on L_f at various time instants in minutes ($Re = 200, L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)

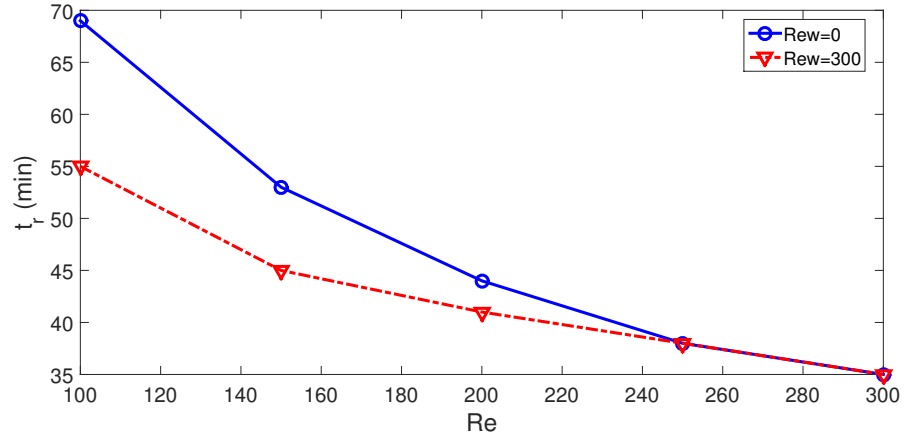


(a) $\text{Rew}=0$

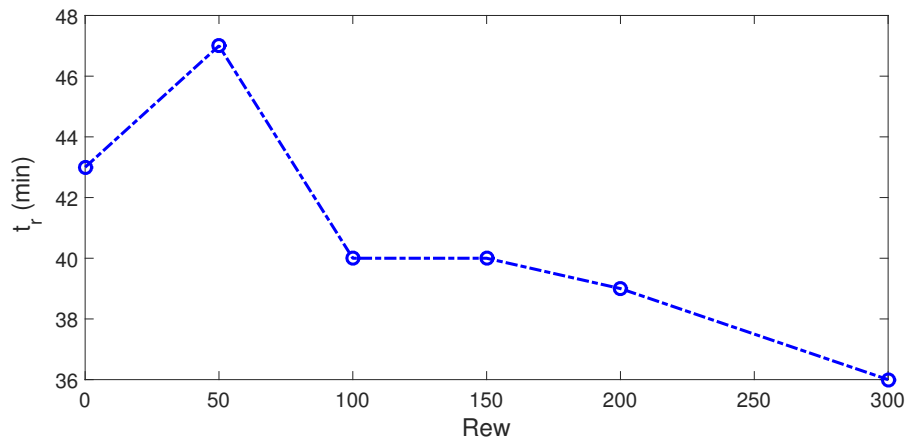


(b) $\text{Rew}=300$

Figure 10: Time evolution of F_r for different Re at two different values of Rew ($\text{Re} = 200, L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)

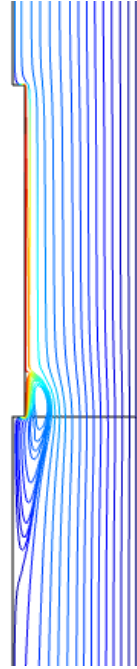


(a)

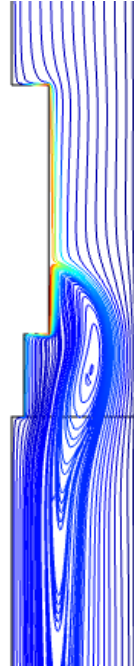


(b) $Re=200$

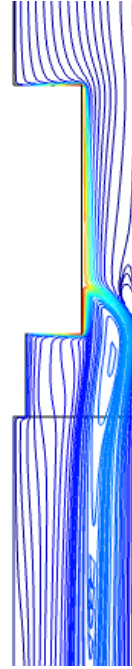
Figure 11: Effects of Re and Rew on the phase transition time ($L1d = 0.1L, L2d = 0.5L, H2d = 0.3H2$)



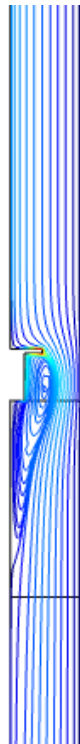
(a) $L2d=0.1L$



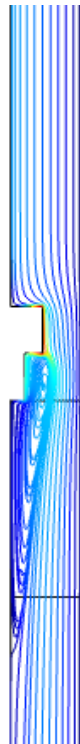
(b) $L2d=0.3L$



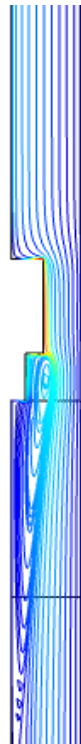
(c) $L2d=0.55L$



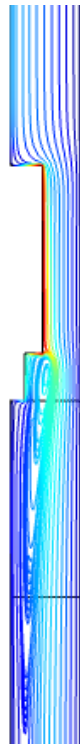
(d) $H2d=0.001H2$



(e) $H2d=0.01H2$

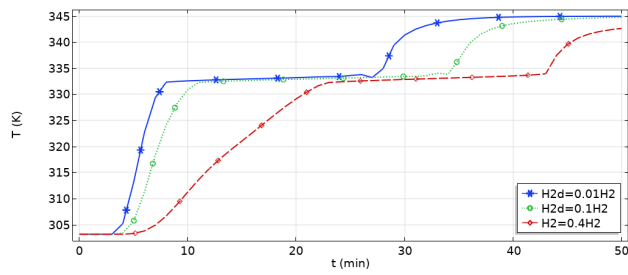


(f) $H2d=0.02H2$

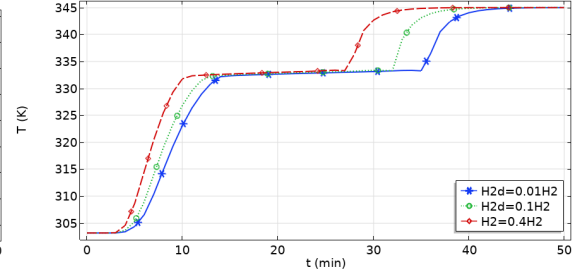


(g) $H2d=0.04H2$

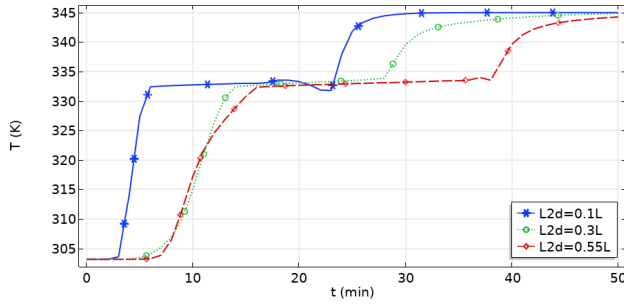
Figure 12: Effects of rotating disk length and height on the flow patterns ($Re = 200$, $Re_w=250$, $L1d=0.1L$)



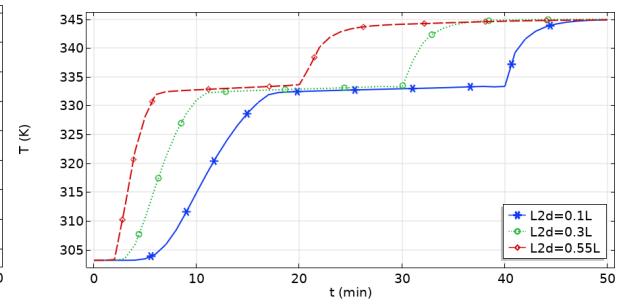
(a) mid point



(b) wall point

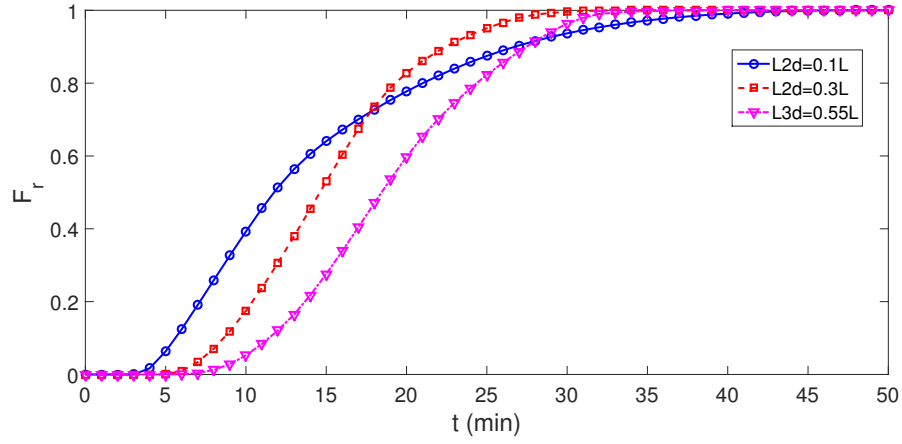


(c) mid point

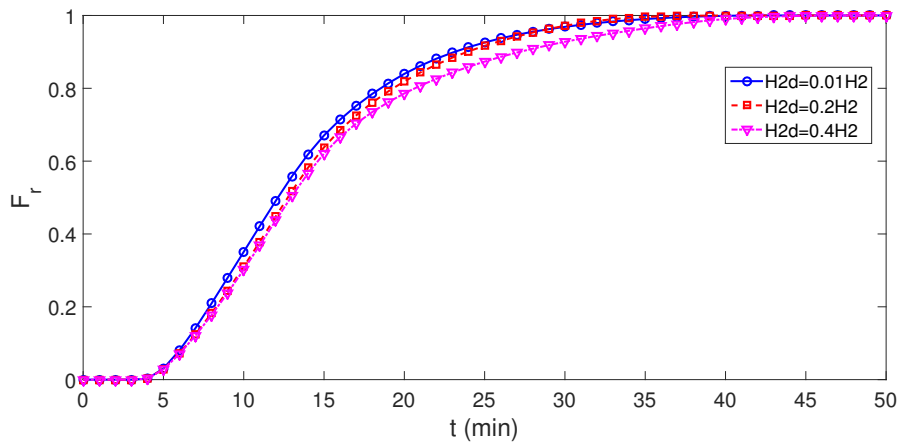


(d) wall point

Figure 13: Effects of inner rotating disk height (a-b) and length (c-d) on the PCM temperature variations ($Re = 200$, $Re_w=250$, $L1d=0.1L$)

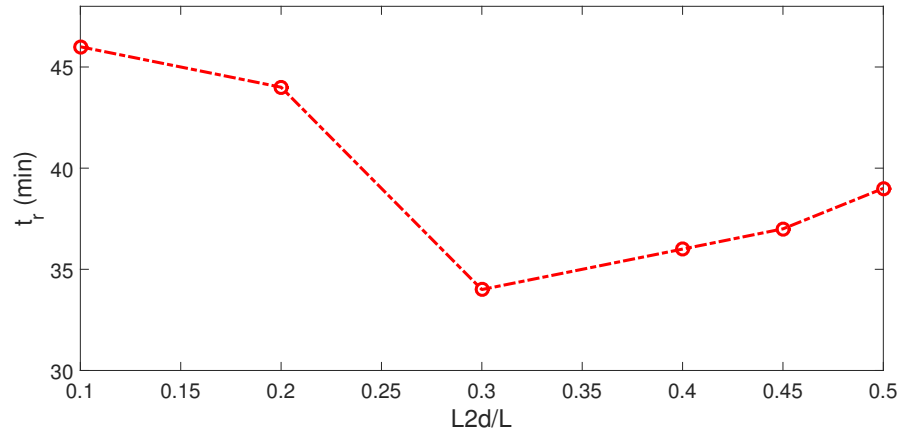


(a)

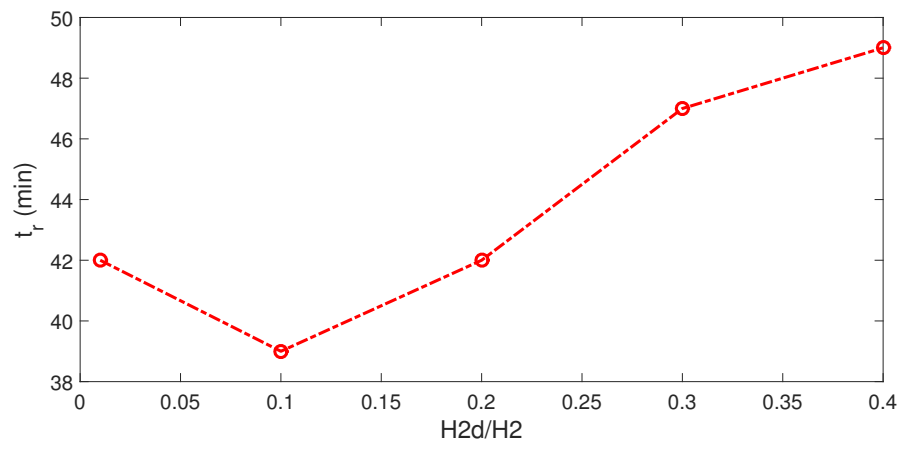


(b)

Figure 14: Time evolution of F_r for different length (a) and height (b) of the inner rotating disk ($Re = 200$, $Re_w=250$, $L1d=0.1L$)



(a)



(b)

Figure 15: Impacts of full phase transition time for different length (a) and height (b) of the inner rotating disk ($Re = 200$, $Re_w=250$, $L1d=0.1L$)

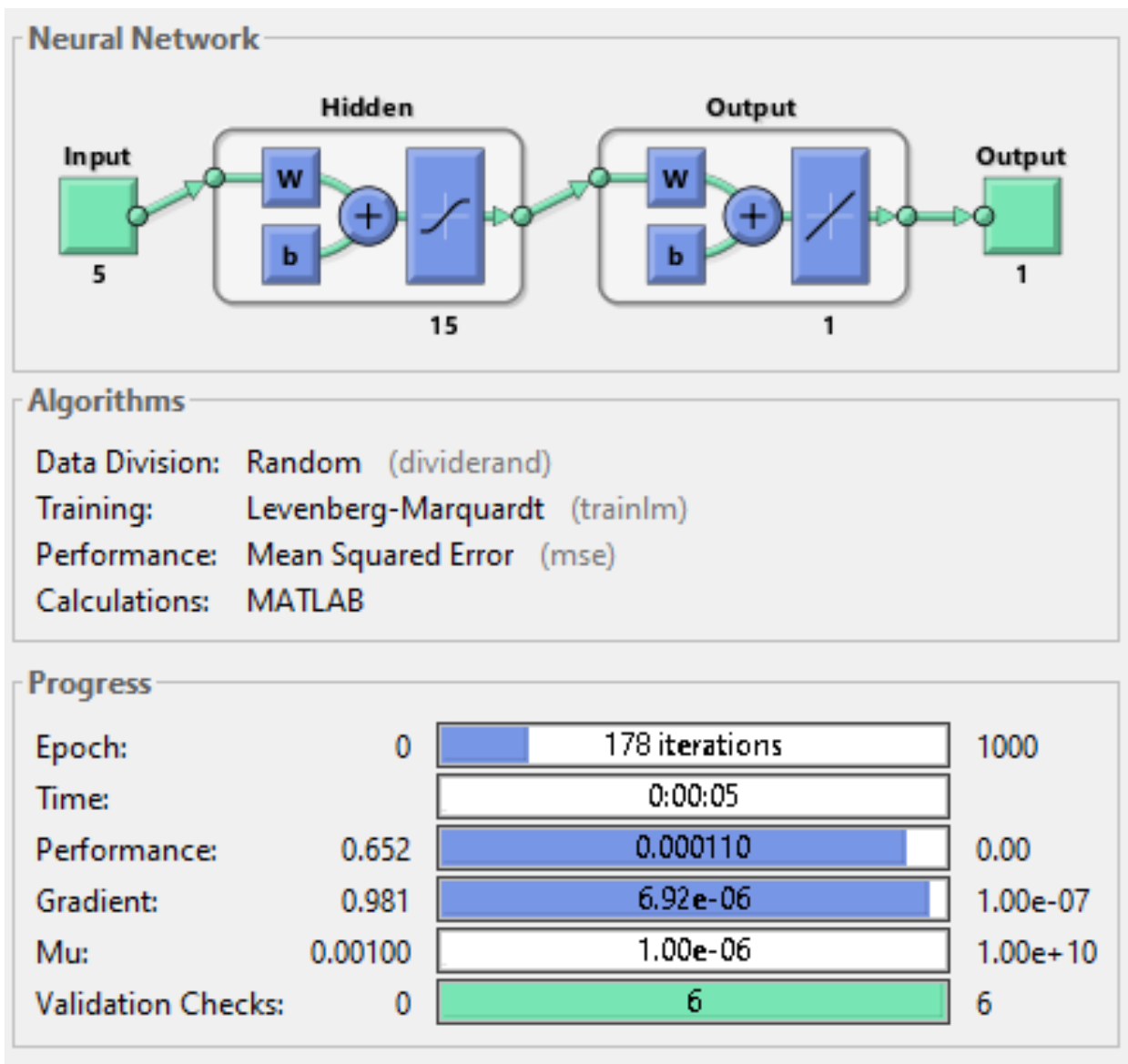
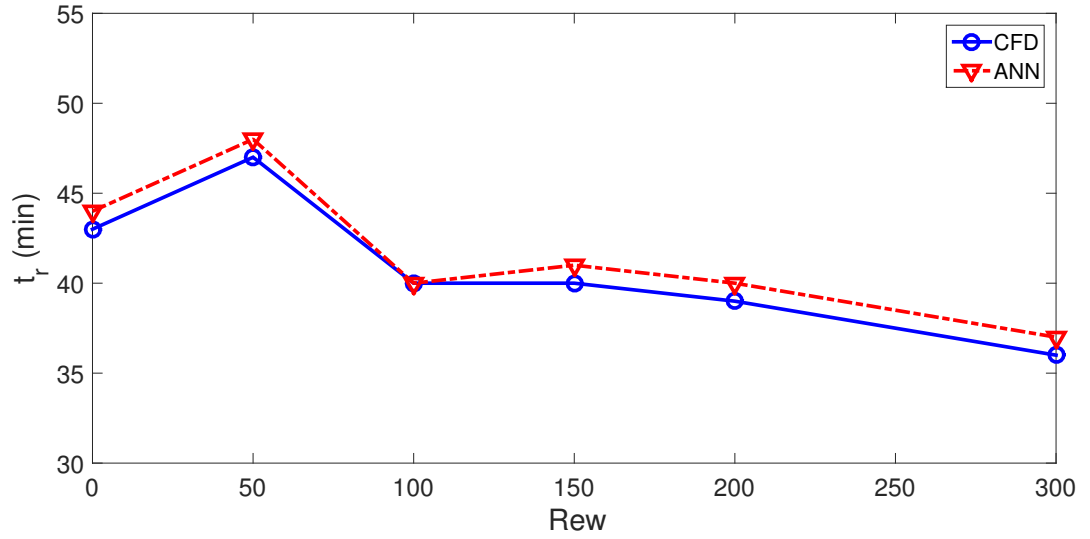
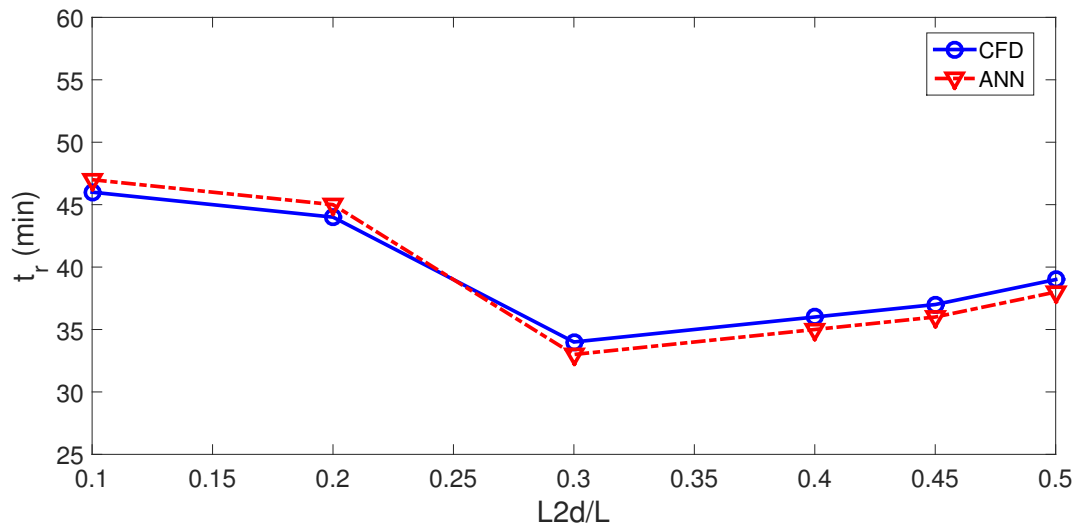


Figure 16: ANN model properties



(a)



(b) Re_w=300

Figure 17: Comparisons of ANN and CFD results in predicting the full phase transition time for varying Re_w (b)